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⑤⑥ References cited :
DE-A- 2 921 330
FR-A- 1 272 980
FR-A- 1 443 905
FR-A- 2 114 718
FR-A- 2 143 791
FR-A- 2 169 718
FR-E- 69 067
GB-A- 565 465
GB-A- 711 364
GB-A- 930 767
GB-A- 1 263 151
US-A- 3 047 373

⑤⑥ References cited :
US-A- 3 337 313
RöMPPS - Chemie - Lexikon - 8. Edition page 1271
S. R. Reddy and M. L. McMillan
"Understanding the effectiveness of Diesel Fuel Flow Improvers" SAE-paper 811181, 1981
H. Vogel "Entwicklung, Wirkung und praxisnahe Prüfung von Fließverbesserern für Mitteldistillate auf unterschiedlicher chemischer Basis" 26. DMK-Conference, 4-6 10.1978, Berlin pages 740-779

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EP 0 061 895 B2

Description

Additive systems for treating distillate fuel oil to improve the flow of wax cloudy fuels through pipe-lines and filters in cold weather are known, as shown by the following patents.

5 United Kingdom Patents 900202 and 1263152 relate to the use of low molecular weight copolymers of ethylene and unsaturated esters especially vinyl acetate, whilst United Kingdom patent 1374051 relates to the use of an additive system which both raises the temperature at which wax crystallisation starts and limits the size of the wax crystals. The use of lower molecular weight copolymers of ethylene and other olefins as pour point depressants for distillate fuels is described in U.K. Patents 848777, 993744 and 1068000 and United States
10 Patent 3679380. Various other special types of polymers are suggested as additives for distillate fuels in United States Patents 3374073, 3499741, 3507636, 3524732, 3608231 and 3681302.

It has also been proposed that combinations of additives may be used in distillate fuels to further improve their flow and pour point properties. For example, United States Patent 3661541 is concerned with the use of combinations of the ethylene/unsaturated ester copolymers types of additive and low molecular weight ethylene/propylene copolymer of U.K. Patent 993744.
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U.S. Patent 3,658,493 teaches various nitrogen salts and amides of acids such as mono and dicarboxylic acids, phenols, and sulfonic acids in combination with ethylene homo or copolymeric pour point depressants for middle distillate oils. U.S. Patent 3,982,909 teaches that nitrogen compounds such as amides, diamides and ammonium salts of monoamides or monoesters of dicarboxylic acids, alone or in combination with petroleum derived microcrystalline wax and/or a pour point depressant, particularly an ethylene backbone, polymeric pour point depressant, are wax crystal modifiers and cold flow improvers for middle distillate fuel oils, including diesel fuel.
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U.S. Patents 3,444,082 and 3,946,093 teach the use of various amides and amine salts of alkenyl succinic anhydride in combination with ethylene copolymer pour point depressants, for distillate fuels.

25 U.S. Patents 3,762,888 teaches a flow improver additive for middle distillate fuels containing a first component polymer such as an ethylene copolymer and as a second component a variety of organic compounds characterised as containing a straight chain polymethylene segment being selected from the group of fatty esters of polyols, alkoxyated polyethers, alkanol esters and the like. Most importantly, with regard to the present invention, this U.S. Patent reports that the second component is one which generally yields little or no flow-improving properties when used in the absence of the polymeric first component. GB-A-930 767 describes additives consisting of one or more diesters of a glycol or a polyglycol containing 2 to 10 carbon atoms and a saturated fatty acid having at least 10 carbon atoms, and their use for lowering the pour point of fuel blends comprising substantial amounts of residual fuel oil diluted with a gas oil. Preferred glycols mentioned are monoethylene glycol, diethylene glycol, triethylene glycol and propylene glycol, and the preferred and only exemplified additive is the diester of diethylene glycol and wool grease stearine.
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The present invention is based upon the discovery that a certain category of polyoxyalkylene esters, ethers, ether/esters and mixtures thereof are effective per se as flow improvers for certain distillate fuels and are especially effective and can be used as the sole additive for narrow boiling distillate fuels (as hereinafter described) which in many cases are unresponsive to conventional flow improver additives. The use of such narrow boiling distillates is increasing due to demands upon refineries to produce more distillates in the kerosene range which raises the initial boiling point of the middle distillate and thus requires a reduction in the final boiling point of the distillate in order to meet cloud point specifications. These narrow boiling distillates therefore have a relatively higher initial boiling point and a relatively lower final boiling point. Whilst additives of the prior art are useful, generally speaking, in distillate fuel oils boiling in the range of 120°C to 500°C, especially 160°C to 400°C, for controlling the growth of separating wax crystals there is a need for further improvement. It has, however, been found difficult to improve the flow and filterability of distillate oils having a relatively narrow boiling range. It has now been found that certain polyalkylene esters, ethers, ester/ethers or mixtures thereof are especially useful in treating narrow boiling distillate fuels to improve their flow properties. The term "narrow boiling distillate" is meant to include those distillate fuels boiling in the range of 200°C ± 50°C to 340°C ± 20°C; fuels having boiling characteristics outside this range being referred to as broad boiling distillates.
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The present invention therefore provides the use as a flow improver additive for distillate fuel oil boiling in the range 120° to 500°C, especially narrow boiling distillate fuel oils, of from 0.0001 to 0.05 wt.% based on the weight of fuel of polyoxyalkylene esters, ethers, ester/ethers and mixtures thereof containing at least two C₁₀ to C₃₀ linear saturated alkyl groups and a polyoxyalkylene glycol of molecular weight 200 to 2,000, the alkylene group of said polyoxyalkylene glycol containing from 1 to 4 carbon atoms.

In addition the invention provides a middle distillate fuel oil having a boiling range from 120°C to 500°C containing 0.0001 to 0.05 wt.%, preferably 0.001 to 0.5 wt.%, of an ester, ether, ester/ether or mixture thereof of the general formula



where R and R¹ are the same or different and may be



the alkyl group being linear and saturated and containing 10 to 30 carbon atoms, and A is a polyoxyalkylene glycol of molecular weight 200 to 2,000 wherein the alkylene group contains 1 to 4 carbon atoms such as a polyoxymethylene, polyoxyethylene or polyoxytrimethylene moiety which is substantially linear; some degree of branching with lower alkyl side chains (such as in polyoxypropylene glycol) may be tolerated but in order to achieve the objective of the invention the glycol should be substantially linear.

Suitable glycols generally are the substantially linear polyethylene glycols (PEG) and polypropylene glycols (PPG) having a molecular weight of 200 to 2,000, which is especially useful for improving the flow properties of narrow boiling distillates.

Esters are the preferred additives of this invention and fatty acids containing about 10-30 carbon atoms are useful for reacting with the glycols for form the ester additives of the present invention but where the additive is to be used in narrow boiling distillates it is preferred to use a C₁₈-C₂₄ fatty acid, especially behenic acid or mixtures of stearic and behenic acids, the esters may also be prepared by esterifying polyethoxylated fatty acids or polyethoxylated alcohols.

Polyoxyalkylene diesters, diethers, ether/esters and mixtures thereof are suitable as additives with diesters preferred for use in narrow boiling distillates. Whilst minor amounts of monoethers and monoesters may also be present and are often formed in the manufacturing process, it is important for additive performance that a major amount of the dialkyl compound is present. In particular stearic or behenic diesters of polyethylene glycol, polypropylene glycol or polyethylene/polypropylene glycol mixtures are preferred.

Therefore, a preferred embodiment of the present invention provides narrow boiling distillate fuels as hereinbefore defined which are improved in their flow and filterability properties containing as a flow improver the ester, ether or ester/ether of a polyethylene glycol or polypropylene glycol of molecular weight 200 to 2,000 and a C₁₈-C₂₄ fatty acid in an amount of from about 0.0001 to 0.05 wt%, preferably in the range of 0.005 to 0.05 wt % based upon the weight of the fuel being treated. Where a polyethylene glycol derivative is used we prefer the polyethylene glycol to have a molecular weight from 200 to 1500, where a polypropylene glycol is used we prefer it has a molecular weight from 200 to 2000. Most preferably the polyalkylene glycol has a molecular weight from 200 to 800.

The polyoxyalkylene esters, ethers or ether/esters may be used as sole additive or in conjunction with other additives. With narrow boiling distillates which are known to be generally unresponsive to conventional additives the polyoxyalkylene esters, ethers or ester/ethers of the present invention are frequently effective as sole additives. In broad boiling distillate fuels, however, the ester, ether or ester/ether additives of the present invention are preferably used in combination with other flow improver additives.

In another aspect, the present invention comprises a distillate fuel boiling in the range 120° to 500°C containing 0.0001 to 0.05 wt.% of a combination cold flow improver additive comprising (i) an ester, ether, ester/ether or mixtures thereof of the general formula



where R and R¹ are the same or different and may be

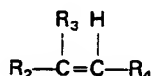


the alkyl group being linear and saturated and containing 10 to 30 carbon atoms, and A is a polyoxyalkylene glycol of molecular weight 200 to 2,000 wherein the alkylene group contains 1 to 4 carbon atoms and (ii) an ethylene copolymer wax crystal growth inhibitor or a C₃₀-C₃₀₀ oil soluble polar nitrogen compound wax crystal growth inhibitor being an amine and/or amide salt and or ester/amide of a carboxylic acid having 1 to 4 carboxylic acid groups or an anhydride thereof.

The ethylene copolymer wax crystal growth inhibitor is typically characterized as a copolymer of Vapor Pressure Osmometric (V.P.O.) Mn 500 to 10,000 containing 3 to 40, preferably 4 to 20 moles of ethylene per

mole of a second ethylenically unsaturated monomer. The ethylene/vinyl acetate copolymer flow improvers are especially preferred. Combinations made up of 90 to 10, preferably 50 to 10 more preferably about 20%-40% by wt polyoxyalkylene ester, ether, ester/ether or mixture of this invention and 10 to 90, preferably 50 to 90 more preferably about 80% to 60% by wt of the ethylene/ unsaturated ester copolymer are preferred. The ethylene/ vinyl acetate copolymers, especially those containing 10 to 40 wt.% more preferably containing about 25 to 35 wt.% vinyl acetate, and having a vapour pressure osmometry (VPO) number average molecular weight of about 1,000 to 6,000, preferably 1500 to 4500 are the preferred co-additives. The dibehenate of polyethylene glycol of molecular weight 200 to 1500 especially 800 to 1500 is a preferred glycol ester for use in such combinations.

The unsaturated monomers which may be copolymerized with ethylene, include unsaturated mono and diesters of the general formula:



wherein R_3 is hydrogen or methyl; R is a $-\text{OOCR}_5$ group wherein R_5 is hydrogen or a C_1 to C_{28} , more usually C_1 to C_{17} , and preferably a C_1 to C_8 , straight or branched chain alkyl group; or R_2 is a $-\text{COOR}_5$ group wherein R_5 is as previously described but is not hydrogen and R_4 is hydrogen or $-\text{COOR}_5$ as previously defined. The monomer, when R_2 and R_4 are hydrogen and R_2 is $-\text{OOCR}_5$, includes vinyl alcohol esters of C_1 to C_{29} , more usually C_1 to C_{18} , monocarboxylic acid, and preferably C_2 to C_5 monocarboxylic acid. Examples of such esters include vinyl acetate, vinyl isobutyrate, vinyl laurate, vinyl myristate and vinyl palmitate; vinyl acetate being the preferred vinyl ester. When R_2 is $-\text{COOR}_5$ and R_3 is hydrogen, such esters include methyl acrylate, isobutyl acrylate, methyl methacrylate, lauryl acrylate, C_{13} Oxo alcohol esters of methacrylic acid, etc. Examples of monomers where R_3 is hydrogen and R_2 and R_4 are $-\text{COOR}_5$ groups, include mono and diesters of unsaturated dicarboxylic acids such as mono C_{13} Oxo fumarate, di- C_{13} Oxo fumarate, diisopropyl maleate, di-lauryl fumarate and ethyl methyl fumarate.

The above-mentioned C_{30} - C_{300} nitrogen compounds are preferably C_{50} - C_{150} amine salts and/or amides formed by reaction of at least one molar proportion of hydrocarbyl substituted amines with a molar proportion of hydrocarbyl acid having 1-4 carboxylic acid groups or their anhydrides; ester/amides may also be used. These nitrogen compounds are described in U.S. Patent 4,211,534. Suitable amines are usually long chain C_{12} - C_{40} primary, secondary, tertiary or quaternary amines or mixtures thereof but shorter chain amines may be used provided the resulting nitrogen compound is oil soluble and therefore normally containing about 30 to 300 total carbon atoms. The nitrogen compound should also have at least one straight chain C_8 - C_{40} alkyl segment.

Suitable amines include primary, secondary, tertiary or quaternary, but preferably are secondary. Tertiary and quaternary amines can only form amine salts. Examples of amines include tetradecyl amine, cocoamine, hydrogenated tallow amine and the like. Examples of secondary amines include dioctadecyl amine, methyl-behenyl amine and the like. Amine mixtures are also suitable and many amines derived from natural materials are mixtures. The preferred amine is a secondary hydrogenated tallow amine of the formula HNR_1R_2 wherein R_1 and R_2 are alkyl groups derived from hydrogenated tallow fat composed of approximately 4% C_{14} , 31% C_{16} , 59% C_{18} .

Examples of suitable carboxylic acids for preparing these nitrogen compounds (and their anhydrides) include cyclohexane dicarboxylic acid, cyclohexene dicarboxylic acid, cyclopentane dicarboxylic acid, dialphanaphthyl acetic acid, naphthalene dicarboxylic acid and the like. Generally these acids will have about 5-13 carbon atoms in the cyclic moiety. Preferred acids useful in the present invention are benzene dicarboxylic acids such as phthalic acid, terephthalic acid, and ortho-phthalic acid. Ortho-phthalic acid or its anhydride is the particularly preferred embodiment.

It is preferred that the nitrogen containing compound have at least one straight chain alkyl segment extending from the compound containing 8-40, preferably 14-24 carbon atoms. Also at least one ammonium salt, amine salt or amide linkage is required to be present in the molecule. The particularly preferred amine compound is that amide-amine salt formed by reacting 1 molar portion of phthalic anhydride with 2 molar portions of di-hydrogenated tallow amine. Another preferred embodiment is the diamide formed by dehydrating this amide-amine salt.

Combinations found especially effective in broad boiling distillate fuels are those containing about 10 to 90 wt.%, preferably 50 to 80 wt.% more preferably 60 to 80 wt.% of the aforesaid nitrogen compound and about 90 to 10 wt.% preferably 50 to 20 wt.% more preferably 20 to 40 wt.% of the polyoxyalkylene ester, ether, ether/ester or mixtures thereof used as the additives of this invention and such a combination and fuels con-

taining such a combination are further embodiments of the present invention.

According to a further embodiment of the present invention the fuel oil composition may also contain a lube oil pour depressant. This has been found particularly useful in improving the flow properties of distillate fuels having higher final boiling points especially those with final boiling points above 385°C. Examples of the preferred lube oil pour depressants are alkyl aromatics such as those made by the Friedel Crafts condensation of a halogenated wax, preferably a straight chain wax with an aromatic hydrocarbon such as naphthalene. Typically suitable halogenated waxes are those containing from 15 to 60, e.g., 160 to 50 carbon atoms and from 5 to 25 wt.% preferably 10 to 18 wt.% halogen, preferably chlorine.

Alternatively the lube oil pour depressant may be the well known oil soluble esters and/or higher olefin polymers and if so it will generally have a number average molecular weight in the range of about 1000 to 200,000, e.g., 1,000 to 100,000, preferably 1000 to 50,000, as measured, for example, by Vapor Pressure Osmometry such as by a Mechrolab Vapor Pressure Osmometer, or by Gel Permeation Chromatography. These second polymers including copolymers with other unsaturated monomers, e.g. olefins, other than ethylene. Typical polymers are described in published United Kingdom Patent Application 2023645 A.

The relative proportions of the polyoxyalkylene ester, ether, or ester/ether the lube oil pour depressant and any other additives that should be used will depend upon inter alia the nature of the fuel. We prefer, however, to use from 0 to 50 wt.% preferably from 5 wt.% to 30 wt.% of the lube oil pour depressant based on the total amount of additive present in the distillate fuel the fuel may also contain from 0 to 90 wt.% of other additives of the types herein described.

The additive systems of the present invention may conveniently be supplied as concentrates of the ester, ether, ester/ether or mixtures thereof of the polyoxyalkylene glycol in oil for incorporation into the bulk distillate fuel. These concentrates may also contain other additives as required. These concentrates preferably contain from 3 to 75 wt.%, more preferably 3 to 60 wt.%, most preferably 10 to 50 wt.% of the additives preferably in solution in oil. Such concentrates are also within the scope of the present invention.

In summary the present invention includes distillate fuel oil boiling in the range about 120°C to 500°C including narrow boiling distillates boiling in the range 200°C \pm 50°C to 340°C \pm 20°C improved in low temperature flow properties by 0.0001 to 0.05 wt.% e.g. 0.001 to 0.5 wt.% of a flow improver comprising 10 to 100 wt.% of a polyoxyalkylene material which is an ester, ether, ether/ester or mixtures thereof containing at least two C₁₀ to C₃₀ linear saturated alkyl groups and a polyoxyalkylene glycol of molecular weight 200 to 2000, the alkylene group in said polyoxyalkylene containing 1 to 4 carbon atoms.

0 to 90 wt.% e.g. 50 to 90 wt.% of an ethylene other unsaturated monomer e.g. vinyl acetate copolymer

0 to 90 wt.% e.g. 50 to 90 wt.% of a C₃₀-C₃₀₀ oil soluble polar nitrogen compound being an amine and/or amide salt and/or ester/amide of a carboxylic acid having 1 to 4 carboxylic acid groups or an anhydride thereof

0 to 50 wt.% e.g. 5 to 30 wt.% of a lube oil pour depressant

The flow improver may be solely the polyoxyalkylene material or any combination of the polyoxyalkylene material with one or more of the other components described above. Other additives may be present also.

The invention is further illustrated by the following examples which are not to be considered as limitative of its scope.

In the Examples the fuels that were used in the tests had the properties, set out in Table 1.

TABLE 1

	Fuel	A	B	C	D	E	F	G	H	I
5	Cloud point (°C)	-9	-9	-4	-2	1	-4	0	—	—
	Wax appearance point, WAP (°C)	-10	-10	-7	-5	-2.5	-5.5	-4	-0.5	1.5
	CFPP (°C)—(untreated)	-12	-12	-6	-5	-3	-5	-4	—	—
10	Wt.% aromatics (FIA)*	18	31	40	28	30	31	23	38	29
	Wax content (wt.%), 5°C below WAP	2.2	1.5	2.2	4.0	0.9	1.0	1.6	0.9	0.9
15	ASTM D86 distillation Initial boiling point, °C	220	180	221	202	182	180	156	161	167
	Final boiling point, °C	341	332	348	343	385	368	355	381	387

*Fluorescence indicator analysis

The fuels are typical of European heating and diesel fuels. Fuels A, B, C and D are examples of Narrow Boiling Distillates (NBD's), while E, F, H and I are examples of Broader Boiling Distillates (BBD's) and G is on the borderline between Narrow and Broad boiling.

By one method, the response of the oil to the additives was measured by the Cold Filter Plugging Point Test (CFPPT) which is carried out by the procedure described in detail in "Journal of the Institute of Petroleum", Volume 52, Number 510, June 1966, pp. 173-185. This test is designed to correlate with the cold flow of a middle distillate in automatic diesels.

In brief, a 40 ml sample of the oil to be tested is cooled in a bath which is maintained at about -34°C to give non-linear cooling at about 1°C/min. Periodically (at each one degree Centigrade drop in temperature starting from at least 2°C above the cloud point) the cooled oil is tested for its ability to flow through a fine screen in a prescribed time period using a test device which is a pipette to whose lower end is attached an inverted funnel which is positioned below the surface of the oil to be tested. Stretched across the mouth of the funnel is a 350 mesh screen having an area defined by a 12 millimetre diameter. The periodic tests are each initiated by applying a vacuum to the upper end of the pipette whereby oil is drawn through the screen up into the pipette to a mark indicating 20 ml of oil. After each successful passage the oil is returned immediately to the CFPP tube. The test is repeated with each one degree drop in temperature until the oil fails to fill the pipette within 60 seconds. This temperature is reported as the CFPP temperature. The difference between the CFPP of an additive free fuel and of the same fuel containing additive is reported as the CFPP depression by the additive. A more effective additive flow improver gives a greater CFPP depression at the same concentration of additive.

Another determination of flow improver effectiveness is made under conditions of the flow improver distillate operability test (DOT test) which is a slow cooling test designed to correlate with the pumping of a stored heating oil. The cold flow properties of the described fuels containing the additives were determined by the DOT test as follows. 300 ml of fuel are cooled linearly at 1°C/hour to the test temperature and the temperature then held constant. After 2 hours at the test temperature, approximately 20 ml of the surface layer is removed by suction to prevent the test being influenced by the abnormally large wax crystals which tend to form on the oil/air interface during cooling. Wax which has settled in the bottle is dispersed by gentle stirring, then a CFPPT filter assembly is inserted. The tap is opened to apply a vacuum of 500 mm of mercury (66661 Pa), and closed when 200 ml of fuel have passed through the filter into the graduated receiver, A PASS is recorded if the 200 ml are collected within ten seconds through a given mesh size or a FAIL if the flow rate is too slow indicating that the filter has become blocked.

CFPPT filter assemblies with filter screens of 20, 30, 40, 60, 80, 100, 120, 150, 200, 250 and 350 mesh number are used to determine the finest mesh (largest mesh number) the fuel will pass. The larger the mesh number that a wax containing fuel will pass, the smaller are the wax crystals and the greater the effectiveness of the additive flow improver. It should be noted that no two fuels will give exactly the same test results at the same treatment level for the same flow improver additive, and, therefore, actual treat levels will vary somewhat from fuel to fuel.

In the Examples the distillate flow improver A1 used was a concentrate in an aromatic diluent of about 50 wt.% of a mixture of two ethylene-vinyl acetate copolymers, having different oil solubilities, so that one func-

tioned primarily as a wax growth arrestor and the other as a nucleator, in accord with the teachings of U.K. Patent 1374051 and its corresponding U.S. Patent 3961916. More specifically, the two polymers are in a ratio of about 75 wt.% of wax growth arrestor and about 25 wt.% of nucleator. The wax growth arrestor consists of ethylene and about 38 wt.% vinyl acetate, and has a number average molecular weight of about 1800 (VPO). It is identified in said U.K. Patent 1374051 as Copolymer B of Example 1 (column 8, lines 25-35) and the corresponding United States Patent 3961916, column 8, line 32. The nucleator consists of ethylene and about 16 wt.% vinyl acetate and has a number average molecular weight of about 3000 (VPO). It is identified in said U.K. Patent 1374051 as copolymer H (see Table 1, columns 7-8) and the corresponding United States Patent 3961916, column 8, line 45. Distillate flow improver A2 was the wax growth arrestor component of A1 used on its own.

Polyethylene glycol (PEG) esters and polypropylene glycol (PPG) esters were prepared by mixing one molar proportion of the glycol with one or two molar proportions of the carboxylic acids for the "mono" and "di" esters respectively. Para-toluene sulphonic acid was added at 0.5 wt.% of the reactant mass as catalyst. The mixture was heated to 150°C with stirring and a slow stream of nitrogen to distill off water of reaction. When the reaction was completed, as judged by the infrared spectrum, the product was poured out while molten and allowed to cool, giving a waxy solid. Elemental analysis, gel permeation chromatography, saponification, and spectroscopic techniques identified the products.

PEG's and PPG's are usually referred to in combination with their molecular weights, e.g. PEG 600 is a 600 average molecular weight polyethylene glycol. This nomenclature has been continued here to the esters so PEG 600 dibehenate is the ester product of the reaction of two molar proportions of behenic acid with one mole of PEG 600. Mixtures of PEG's of different molecular weights may also be used, e.g. mixed PEG (200/400/600) distearate is the distearate ester of a 1:1:1 by weight mixture of PEG's 200, 400 and 600. Mixtures of carboxylic acids may also be used, e.g. PEG di(stearate/behenate) is the product from one mole PEG with one mole each of stearic and behenic acids. In both types of mixtures, 2, 3 or several different PEG's, PPG's, PE/PP-G copolymers, and carboxylic acids may be used.

As examples of polar, monomeric, nitrogen containing growth inhibitors, the following compounds designated hereinbelow as "B1", "B2", "B3" and "B4" were used:

B1: The reaction product of one mole of phthalic anhydride with two moles of dihydrogenated tallow amine, to form a half amine/half amide salt.

B2: The phthalic diamide prepared by removing one mole of water per mole of B1.

B3: The di-hydrogenated tallow amine salt of monooctadecyl phthalate.

B4: The diamide product of reaction and dehydration of two moles of di-hydrogenated tallow amine with one mole of maleic anhydride.

Although many of the additives are available as oil solutions active ingredient (a.i.) as used in the Examples refers to actual amount of additive.

Example 1

The performance in the CFPP test of normally difficult to treat narrow boiling distillate fuels containing poly-oxyalkylene esters of the present invention was compared with those of the same fuels containing ethylene vinyl acetate (EVA) copolymeric additives, with the following results:

	Flow improver	ppm of active ingredient	CFPP depression*			
			Fuel of Table 1			
			A	B	C	D
5	A1	100	-1	0	—	0
	A1	500	-1	-1	—	0
10	A2	100	-1	0	0	-1
	A2	500	-1	2	1	0
	PEG 600 di-behenate	100	3	3	4	4
15	Mixed PEG (200/400/600) di(stearate/behenate)	100	4	4	.5	2
	Tween 65	500	1	1	—	0

*A negative value indicates an elevation of the CFPP.
 Tween 65 is a polyethoxylated sorbitan tristearate (non-linear).

These results show that in these fuels, significant CFPP depression may be produced by only 100 ppm of PEG ester while 500 ppm of EVA is ineffective.

Example 2

The performance of the fuels used in Example 1 containing certain polyglycol esters of the present invention was compared in the DOT test at 5°C to 7°C below the fuel WAP (as given in Table 1) with certain commercially available flow improvers with the following results.

	Parts per million of flow improver in fuel	Fuel					
		A		B		C	
		100	500	100	500	100	500
	Flow improver						
	None	30		Block 20		Block 20	Block 20
40	A2	30	60	20	40	—	40
	""Keroflux"" H	30	60	B20	40	—	—
	A1	20	60	40	20	—	60
45	""Keroflux"" M	B20	30	B20	40	—	—
	""Tween 65""	60	120	40	30	100	—
	Polyethylene glycol (600) dibehenate	80	120	40	80	—	120
50	Mixed PEG (200/400/600) di-(stearate/behenate)	150	200	60	200	100	150

""Keroflux"" H is an ethylene-vinyl acetate copolymer.

""Keroflux"" M is an ethylene-2-ethylhexyl acrylate copolymer.

""Tween 65"" is a polyethoxylated sorbitan tristearate (non-linear).

""Keroflux"" and ""Tween"" are Registered Trade Marks.

These results show the advantage of the PEG esters as flow improvers when compared with various conventional copolymer flow improvers in these fuels. The advantage of the PEG esters over the non-linear ethoxylated ester, "Tween 65", is also illustrated. "Block 30" or "B20" means the fuel would not pass through a 20 mesh screen.

Example 3

The DOT test was used to determine the performance of Fuel A of Table 1, at -15°C, containing 100 parts per million of various polyoxyethylene dibehenates additives in which the polyoxyethylene segments were of different number average molecular weight.

The results were as follows:

	Polyethylene glycol mol. wt.	Finest mesh passed mesh No.
	No additive	20
	100	40
	144	40
	200	150
	400	100
	600	80
	1,000	30
	1,500	40
	4,000	40

This shows the advantage of those esters of PEG's with molecular weights 200 to 600 which are preferred.

Example 4

Example 3 was repeated but using as the polyglycol ester 100 ppm of the diester of a 600 molecular weight polyethylene glycol which had been esterified with 2 moles of carboxylic acids of different chain lengths.

The results were as follows:

	Polyethylene glycol ester (carbon number)	Finest mesh passed mesh No.
	Laurate (C ₁₂)	20
	Myristate (C ₁₄)	30
	Palmitate (C ₁₆)	40
	Stearate (C ₁₈)	40
	Behenate (C ₂₂)	80
	Stearate/behenate	100
	Mixed PEG 200/400/600 stearate/behenate	150

The mixed stearate/behenate is obtained by reacting the polyethylene glycol with 2 moles of an equi-molar mixture of stearic and behenic acids.

This example shows the advantage of PEG esters of the higher molecular weight carboxylic acids, and also that esters of single or mixed PEG's with mixtures of carboxylic acids can be advantageous.

Example 5

The DOT test was used to compare the flow improving effectiveness of the PEG esters with the PPG esters, and also with mixtures of PPG and PEG esters, in Fuel A or Table 1 (at -15°C).

5

	Ester (molecular wt.)	ppm of Ester (active ingredient)	Finest mesh passed mesh No.
10	(a) Mixed PEG (200/400/600) di-(stearate/behenate)	100 500	150 200
	(b) PPG (400) di-(stearate/behenate)	100 500	20 200
15	(c) PPG (1,025) di-(stearate/behenate)	100 500	30 150
	(d) PPG (2,025) di-(stearate/behenate)	100 500	20 60

20

	Ester mixture (weight ratio)	ppm of a.i.	Finest mesh No. passed
25	(a)/(b)=1/4	500	250
	(a)/(c)=1/4	500	150
	(a)/(d)=1/4	500	150

30 These results show that the PPG distearate/behenates are also very effective flow improvers at higher concentrations but not as effective as the PEG esters at lower concentrations. The effectiveness of the PPG esters also show a dependence on the PPG molecular weight. Mixtures of PPG and PEG esters can also be used effectively.

35 Example 6

The CFPP depression of Fuel D of Table 1 containing PEG esters of various PEG molecular weights and esterified with different carboxylic acids was measured to be as follows:

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	PEG ester	ppm of Active ingredient in fuel D	CFPP depression
5	PEG 600 dilaurate	100	0
	PEG 600 dimyristate	100	0
	PEG 600 dipalmitate	100	0
10	PEG 600 distearate	100	0
	PEG 600 dibehenate	100	5
	PEG 200 dibehenate	100	0
15	PEG 400 dibehenate	100	4
	PEG 600 dibehenate	100	5
	PEG 1,000 dibehenate	100	0
20	PEG 1,500 dibehenate	100	0
	Mixed PEG (200/400/600) dibehenate	100	5
	Mixed PEG (600/1000) dibehenate	100	5

These results show PEG 400 and PEG 600 dibehenates to have both optimum PEG molecular weights and optimum carboxylic acid for CFPP depression in this fuel. For the sake of comparison, the CFPP depression for Fuel D containing 100 ppm of Additive A1 was -1.

Example 7

The effectiveness of blends of PEG esters with other additives in NBD's has been determined by the DOT test, in Fuel B of Table 1 at -15°C. "4/1" is a weight ratio.

	Additive	ppm of Active ingredient	Finest mesh number passed
	PEG 400 dibehenate	100	40
40	B1	500	60
	B1/PEG 400 dibehenate (4/1)	500	200
	B1/Tween 65 (4/1)	500	40
45	A2	500	40
	A2/Mixed PEG di(stearate/behenate) (4/1)	500	60

These results show the advantage of the combination of PEG ester with the polar monomer B1, over either alone and over the B1/Tween 65 combination. The performance of the EVA-copolymer A2, is also improved by the presence of PEG ester.

Example 8

The effectiveness of PEG esters in combination with ethylene/vinyl acetate copolymer growth inhibitor as CFPP depressors in broad boiling Fuel E of Table 1 was found to be as follows:

5	EVA (A2) ppm of polymer	PEG ester		CFPP depression (°C)
		Nature	ppm of active ingredient	
	100	—	0	0
	200	—	0	2
10	80	PEG dibehenate	20	12
	100	"	40	15
	0	"	100	0
	0	"	200	2
15	80	Mix PEG (600/1000) dibehenate	20	13
	160	"	40	18
	0	"	200	2
20	150	C ₂₈ —C ₃₀ mixed PEG ester*	50	16

*Made by the esterification of 1 mole of the mixed PEG (200/400/600) with 2 moles of the saturated carboxylic acid derived from the reaction of C₂₆—C₂₈ alpha olefins with acetic anhydride, in the presence of di-t-butyl-peroxide as catalyst.

These results show- how very effective such combinations are, over the components separately.

Example 9

The effectiveness of PEG esters in combination with polar monomeric compounds as CFPP depressors in Fuel F of Table 1 are found to be as follows:

35	Additive		PEG ester		CFPP depression
	A2 (for comparison)	ppm of a.i.		ppm of a.i.	
		75	—	0	0
40	A2	75	PEG 600 dibehenate	25	10
	A2	75	PEG 600 distearate	25	0
45	B1	75	—	0	0
	B1	75	PEG 600 dibehenate	25	6
	B2	75	—	0	4
50	B2	75	PEG 600 dibehenate	25	7
	B3	75	—	0	2
55	B3	75	PEG 600 dibehenate	25	12

These results show the advantage of the PEG dibehenate over the distearate, when used in combination with A2, and the benefit of using for a component such as PEG 600 dibehenate, in this application. Also that polar monomeric compounds can be effective CFPP depressors when used in combination with the PEG 600

ester.

Example 10

5 In this example the effectiveness of PEG ester/A2 combinations are tested by the DOT test at -12°C.

10	Growth inhibitor ppm (a.i.)		PEG ester		Finest mesh number passed
				ppm of a.i.	
	Fuel E of Table 1				
	A2	200	—	0	150
15	A2	170	PEG 600 dibehenate	30	250
	A2	170	Mixed PEG (400/600/1,000) di- (stearate/behenate)	30	250
	Fuel G of Table 1				
20	A2	500	—	0	40
	A2	400	Mixed PEG (200/400/600) di- (stearate/behenate)	100	150
25	B1	400	"	100	200

These results show the greater effectiveness of combinations of PEG esters with EVA copolymer or polar monomeric wax crystal growth inhibitors over an equivalent concentration of the growth inhibitor alone.

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Example 11

35 In this example, the results are from three 25 m³ tanks of Fuel D of Table 1 which were tested side by side. Over a period of three weeks storage, under natural cold conditions (including natural temperature cycling), the fuel at -13.5°C was pumped out of the tanks as in a fuel distribution situation and the finest filter screen through which fuel would flow was recorded.

	Additive (at 0.1% of active ingredient)	Finest mesh passed
40	(a) A1	40
	(b) Mixed PEG (200/400/600) di(stearate/behenate)	60
45	(c) A2/mixed PEG ester as (b) (3/1 ratio)	80

50 The filter screens usually used in such fuel distribution equipment are of 60 mesh number and so it can be seen that while the fuel containing EVA copolymer A1 gave unsatisfactory performance by blocking a 60 mesh number filter, the fuel containing PEG ester alone and fuel containing an EVA copolymer/PEG ester combination gave satisfactory flow on pumping.

Example 12

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Three barrels of Fuel A of Table 1 were cooled to 0.5°C/hour to -13°C and after a cold soak period, a 300 ml sample of the fuel was tested for its cold flow performance, as in the DOT. The barrels were then slowly heated to above the WAP of the fuel, then cooled again at 0.5°C/hour to -13°C. The fuel was then pumped

out of the barrels through a range of filter screens to determine the finest that the waxy fuel could pass through.

5	Additive	ppm a.i.	Finest mesh passed (mesh No.)	
			First cool	Second cool
	A1	500	60	40
10	Mixed PEG (200/400/600)	100	80	80
	di(stearate/ behenate)	500	120	120
15	Mixed PEG ester (as above)/ PPG (1025) dibehenate	100/400	120	100

The advantage of PEG esters and a PEG ester/PPG ester blend over the ethylene/vinyl acetate copolymer A1 is reconfirmed.

Example 13

The DOT test was used at a test temperature of - 10°C to compare the linear saturated esters with linear unsaturated esters, e.g., an oleic acid ester.

25	Fuel of Table 1	Additive	ppm	Finest mesh passed
30	D	PEG (600) dibehenate	500	100
	D	PEG (600) dioleate	500	Block 20
	D	None	0	Block 20

Example 14

The DOT test was repeated in a series of three broad boiling distillate fuels and illustrates the effectiveness of linear PEG esters even when used alone in such fuels.

Comparative data is provided with the "A2" ethylene-vinyl acetate copolymer as well as with a dioleate ester to show the criticality associated with a linear saturated alkyl ester.

Fuel of Table 1	Additive	ppm	Finest mesh passed
E	A2	200	200
E	PEG (600) dibehenate	200	200
E	PEG (600) dioleate	200	40
E	None	—	30
H	A2	300	100
H	PEG (600) dibehenate	300	100
H	PEG (600) dioleate	300	40
H	None	—	40
I	A2	250	120
I	PEG (600) dibehenate	250	200
I	PEG (600) dioleate	250	80
I	None	—	80

Example 15

A fuel of relative high boiling point having the following characteristics:

Cloud point (°C)	+4
Wax appearance point (°C)	-0.7
CFPP (°C)—untreated	-5
ASTM D86 distillation	
Initial boiling point, °C	185
Final boiling point, °C	386

was treated with varying amounts of an additive mixture comprising a blend of 1 part by weight of PEG (600) dibehenate and 4 parts by weight of additive A2 with the following results:

	Additive treat rate (ppm)	CFPP, °C
5	150	-14
	200	-14
	250	-14
10	300	-14
	350	-16
	450	-16
15	500	-16
	550	-7
	650	-7

20 In this Example, the CFPP values are the actual temperature at which the fuel failed the CFPP test.
 10 wt.% based on the total weight of additive of a wax naphthalene made by Friedel Crafts condensation
 of about 100 parts by weight of n-paraffin wax having a melting point of about 125-129°F chlorinated to about
 14.5 wt.% chlorine based on weight of chlorinated wax and about 12 parts by weight of naphthalene (known
 as C) was added, and the CFPP performance of the fuels containing the mixture used above were as follows:

	Treat rate	CFPP, °C
25	550 ppm of blend+55 ppm of C	-19
30	650 ppm of blend+65 ppm of C	-20

For example this data shows the further improvement achieved in this fuel by the incorporation of C.

Example 16

35 The DOT test was used with Fuel A at a temperature of -15°C to compare PEG 600 Distearate and PEG
 600 Diisostearate at a treat rate of 200 parts per million of the additive. The results were as follows:

	Additive	P.P.M. a.i.	Finest mesh passed
40	PEG 600 distearate	200	400 mesh
	PEG 600 di-isostearate	200	blocked 20

45 thus showing the benefit of the linear alkyl group.

Example 17

50 Polytetramethylene glycols, "Teracols", of general formula $\text{HO}-(\text{CH}_2)_4-\text{O}_m-\text{H}$ were prepared of molecular
 weights 650, 1000 and 2000 and esterified with two moles of behenic acid. These materials were then tested
 in Fuel A in the DOT test at a temperature of -15°C with the following results.

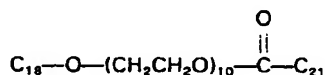
55

Additive	P.P.M. (a.i.)	Finest mesh passed
Teracol (650) dibehenate	200	block 20
Teracol (1000) dibehenate	200	30
Teracol (2000) dibehenate	200	40

Thus showing certain the Teracol derivatives to be active but as comparison with Example 3 shows less active than the comparable PEG and PPG esters.

Example 18

A C₁₈ linear alcohol was ethoxylated and the resulting product esterified with one mole of behenic acid to give an ester ether of the following structure



This additive gave a 80 mesh pass in Fuel A in the DOT test at -15°C and at a concentration of 200 p.p.m.

Example 19

PEG 600 was reacted with 2 moles of succinic acid and this product then reacted with 2 moles of a C₂₂/C₂₄ mixed, straight chain, saturated alcohol to give the product



This was tested in Fuel J which had a cloud point of +4°C, a wax appearance point of 0°C, a CFPP performance of -1°C, an Initial Boiling Point of 195°C and a Final Boiling Point of 375°C. The product was tested in the DOT test at -6°C and the fuel with no additive passed a 40 mesh screen whilst that containing 200 p.p.m. of additive passed an 80 mesh screen.

Incorporating 200 p.p.m. of this additive in fuel A gave a 100 mesh pass at -15°C in the DOT test.

Example 20

The effect of PEG (600) Dibehenate was compared with that of PEG (600) Dierucate in Fuel K which had a cloud point of -2°C; a wax appearance point of -6°C, an Initial Boiling Point of 200°C and a Final Boiling Point of 354°C. The untreated fuel had a CFPP of -7°C which was unaltered by the addition of PEG (600) dierucate but reduced by 4°C by the PEG (600) Dibehenate showing the importance of the alkyl group being saturated.

Example 21

Mixtures of 4 parts of Distillate flow improver A2 and of 1 part of different PEG dibehenates were tested in the CFPP test in Fuel E of the following results.

	Additive	CFPP 100 p.p.m. additive	Depression 200 p.p.m. additive
5	A ₂ Alone	1	2
	EVA PEG ester 4: 1		
10	A ₂ PEG (200) dibehenate	1	2
	A ₂ PEG (400) dibehenate	1	2
	A ₂ PEG (600) dibehenate	13	16
15	A ₂ PEG (1000) dibehenate	14	17
	A ₂ PEG (1500) dibehenate	14	17
	A ₂ PEG (4000) dibehenate	3	3
20	A ₂ PEG (600/1000/1500) dibehenate	14	18
	PEG (600) dibehenate alone	6	
	*P (EO/PO) 8000 dibehenate	0	0

25 *A poly(ethylene oxide/propylene oxide) of 8000 molecular weight condensed with two moles of behenic acid.

Example 22

30 Example 21 was repeated using Teracol derivatives in place of the PEG dibehenates with the following results

	Additive	CFPP depression 100 p.p.m. additive
35	Teracol 650 dibehenate 4:1	3
	*A ₂ Teracol (650) dibehenate	0
40	Teracol (1000) dibehenate	0
	*A ₂ Teracol (1000) dibehenate	3
	Teracol 2000 dibehenate	3
45	*A ₂ Teracol (2000) dibehenate	0

*A ratio of EVA/Teracoldibehenate of 4:1.

Showing the Teracol derivatives to be much less effective than the PEG derivatives.

50

Example 23

Various additives were tested in the DOT test at - 10°C in Fuel L which had a cloud point of -4°C, a wax appearance point of -6°C, an untreated CFPPT of -6°C, an Initial Boiling Point of 216°C and a Final Boiling Point of 353°C. The results were as follows

55

	Additive	P.P.M. (a.i.)	DOT test finest mesh passed
5	None	—	block 20
	PEG (600) dibehenate	100	150
	PEG (600) monobehenate	100	40
10	Teracol (650) dibehenate	100	30
	Teracol (1000) dibehenate	100	20
	Teracol (2000) dibehenate	100	20
15	Poly(E.O./P.O.—8000 molecular weight)	100	20
	Dibehenate	500	20

Example 24

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The CFPP depression of Fuel D containing various additives was found to be as follows:

	Additive	P.P.M. (a.i.)	CFPP depression (°C)
25	PEG 200/400/600 dibehenate	250	4
	$\text{C}_{21}\text{H}_{43}\text{C} \begin{array}{c} \text{---} (\text{OCH}_2\text{CH}_2)_8 \text{OH} \\ \\ \text{O} \end{array}$	250 500	—1 —1
30	$\text{C}_{18}\text{H}_{37}\text{---O---}(\text{CH}_2\text{CH}_2\text{O})_{10}\text{---H}$	250 500	—2 —5
35	$\text{C}_{18}\text{H}_{37}\text{---O---}(\text{CH}_2\text{CH}_2\text{O})_{10}\text{---C} \begin{array}{c} \text{---C}_{21}\text{H}_{43} \\ \\ \text{O} \end{array}$	250 500	1 3

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Claims

Claims for the following Contracting States : BE, CH, DE, FR, GB, IT, LI, LU, NL, SE

- 45 1. The use as a cold flow improver additive for distillate fuel oil boiling in the range 120° to 500°C of from 0.0001 to 0.05 wt.% based on the weight of the fuel of polyoxyalkylene esters, ethers, ester/ethers or mixtures thereof containing at least two C₁₀ to C₃₀ linear saturated alkyl groups and a polyoxyalkylene glycol of molecular weight 200 to 2,000 the alkylene group of said polyoxyalkylene glycol containing from 1 to 4 carbon atoms.
- 50 2. The use according to claim 1 for distillate fuel oils boiling in the range of 200°C ± 50°C to 340° ± 20°C.
3. The use according to claim 1 or claim 2 wherein the C₁₀ to C₃₀ linear saturated alkyl group is C₁₈ to C₂₄.
- 55 4. A middle distillate fuel oil having a boiling range from 120°C to 500°C containing 0.0001 to 0.05 wt.% of an ester, ether, or ester/ether or mixture thereof of the general formula
- $$\text{R} - \text{O} - (\text{A}) - \text{O} - \text{R}^1$$
- where R and R¹ are the same or different and may be

(i) n-Alkyl



the alkyl group being linear and saturated and containing 10 to 30 carbon atoms and A is a polyoxyalkylene glycol of molecular weight 200 to 2,000 wherein the alkylene group contains 1 to 4 carbon atoms.

5. The composition of claim 4 wherein the fuel oil is a narrow boiling distillate fuel having a boiling range of $200^{\circ}\text{C} \pm 50^{\circ}\text{C}$ to $340^{\circ}\text{C} \pm 20^{\circ}\text{C}$.
6. The composition of claim 4 or 5 wherein R and R¹ contain 18 to 22 carbon atoms.
7. The compositions of claims 4 to 6 wherein the polyoxyalkylene glycol is a polyethylene glycol.
8. The composition of any of claims 4 to 6 wherein the glycol is a mixture of polyethylene and polypropylene glycols.
9. The composition of any of claims 4 to 8 wherein the acid is behenic acid and the glycol has a molecular weight of 200 to 800.
10. The composition of any one of claims 4 to 9 also containing a lube oil pour depressant.
11. The composition of claim 10 wherein the lube oil pour depressant is an alkylated aromatic.
12. A distillate fuel boiling in the range 120° to 500°C containing 0.0001 to 0.05 wt.% of a combination cold flow improver additive comprising (i) an ester, ether, ester/ether or mixtures thereof of the general formula



where R and R¹ are the same or different and may be

(i) n-Alkyl



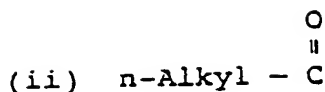
the alkyl group being linear and saturated and containing 10 to 30 carbon atoms and A is a polyoxyalkylene glycol of molecular weight 200 to 2,000 wherein the alkylene group contains 1 to 4 carbon atoms and (ii) an ethylene copolymer wax crystal growth inhibitor or a C₃₀-C₃₀₀ oil soluble polar nitrogen compound wax crystal growth inhibitor being an amine and/or amide salt and/or ester/amide of a carboxylic acid having 1 to 4 carboxylic acid groups or an anhydride thereof.

13. The distillate fuel of claim 12 wherein the ethylene copolymer is an ethylene vinyl acetate copolymer.
14. The distillate fuel of claim 12 and 13 containing from 20 to 40 wt.% of the polyoxyalkylene glycol compound and 80 to 60 wt.% of the ethylene copolymer based on the total weight of additive in the fuel.
15. The distillate fuel of claim 12 wherein the polar nitrogen compound is the reaction product of a C₁₂-C₄₀ secondary amine and phthalic anhydride.
16. The distillate fuel of claim 15 or claim 12 containing from 20 to 40 wt.% of the ester, ether or ester/ether of the polyoxyalkylene glycol and from 80 to 60 wt.% of the C₃₀ to C₃₀₀ oil soluble polar nitrogen compound.
17. An additive concentrate for incorporation into distillate fuel comprising a solution containing from 3 to 75 wt.% of an ester, ether or ester/ether or mixtures thereof of the general formula



where R and R¹ are the same or different and may be

(i) n-Alkyl

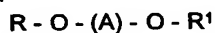


the alkyl group being linear and saturated and containing 10 to 30 carbon atoms and A is a polyoxyalkylene glycol of molecular weight 200 to 2,000 wherein the alkylene group contains 1 to 4 carbon atoms, and also containing an ethylene copolymer wax crystal growth inhibitor or a C₃₀-C₃₀₀ oil soluble polar nitrogen compound wax crystal growth inhibitor being an amine and/or amide salt and/or ester/amide of a carboxylic acid having 1 to 4 carboxylic acid groups or an anhydride thereof.

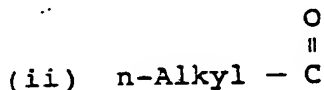
18. An additive concentrate according to claim 17 containing from 3 to 60 wt.% of the ester, ether, ester/ether or mixture thereof.
19. An additive concentrate according to claim 17 or 18 containing from 60 to 80 wt.% based on the total additive content of the concentrate of the ethylene copolymer or C₃₀-C₃₀₀ oil soluble polar nitrogen compound.

Claims for the following Contracting State : AT

1. A process for improving the cold flow of distillate fuel oil boiling in the range 120° to 500° comprising incorporating therein from 0.0001 to 0.05 wt.% of polyoxyalkylene ester, ether, ester/ether or mixtures thereof which contain at least two C₁₀ to C₃₀ linear saturated alkyl group and a polyoxyalkylene glycol of molecular weight 200 to 2,000 the alkylene group of said polyoxyalkylene glycol containing from 1 to 4-carbon atoms.
2. A process according to claim 1 in which the distillate fuel oil boils in the range of 200°C ± 50°C to 340°C ± 20°C.
3. A process according to claim 1 or claim 2 wherein the C₁₀ to C₃₀ is stearic and/or behenic.
4. A process according to any of the preceding claims wherein the polyoxyalkylene glycol is a polyethylene glycol.
5. A process according to any of the preceding claims wherein the glycol is a mixture of polyethylene and polypropylene glycols.
6. A process according to any one of the preceding claims comprising also incorporating into the distillate fuel oil a lube oil pour depressant.
7. A process for improving the cold flow properties of distillate fuels boiling in the range 120° to 500°C comprising incorporating therein from 0.0001 to 0.05 wt.% of a combination of (i) an ester, ether, ester/ether or mixtures thereof of the general formula



where R and R' are the same or different and may be



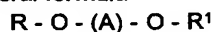
the alkyl group being linear and saturated and containing 10 to 30 carbon atoms and A is a polyoxyalkylene glycol of molecular weight 200 to 2,000 wherein the alkylene group contains 1 to 4 carbon atoms and (ii) an ethylene copolymer wax crystal growth inhibitor or a C₃₀-C₃₀₀ oil soluble polar nitrogen compound wax crystal growth inhibitor being an amine and/or amide salt and/or ester/amide of a carboxylic acid having 1 to 4 carboxylic acid groups or an anhydride thereof.

8. A process according to claim 7 wherein the ethylene copolymer is an ethylene vinyl acetate copolymer.

9. A process according to claim 7 or 8 comprising incorporating from 20 to 40 wt.% of the polyoxyalkylene glycol and 80 to 60 wt.% of the ethylene copolymer or the C₃₀ to C₃₀₀ oil soluble polar nitrogen compound based on the total weight of additive in the fuel.

5 10. A process according to claim 7 wherein the polar nitrogen compound is the reaction product of a C₁₂-C₄₀ secondary amine and phthalic anhydride.

11. A process according to any of the preceding claims wherein the polyoxyalkylene ester, ether or ester/ether is incorporated into the distillate fuel as an oil solution containing from 3 to 75 wt.% of an ester, ether or ester/ether or mixtures thereof of the general formula



where R and R¹ are the same or different and may be

(i) n-Alkyl

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the alkyl group being linear and saturated and containing 10 to 30 carbon atoms and A is a polyoxyalkylene glycol of molecular weight 200 to 2,000 wherein the alkylene group contains 1 to 4 carbon atoms.

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12. A process according to claim 11 in which the oil solution also contains an ethylene copolymer wax crystal growth inhibitor or a C₃₀-C₃₀₀ oil soluble polar nitrogen compound wax crystal growth inhibitor being an amine and/or amide salt and/or ester/amide of a carboxylic acid having 1 to 4 carboxylic acid groups or an anhydride thereof.

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13. A process according to claim 12 in which the oil solution contains from 60 to 80 wt.% based on the total additive content of the concentrate of the ethylene copolymer or C₃₀-C₃₀₀ oil soluble polar nitrogen compound.

Patentansprüche

35

Patentansprüche für folgende Vertragsstaaten : BE, CH, DE, FR, GB, IT, LI, LU, NL, SE

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1. Verwendung als Kaltfließverbesserungsadditiv für Destillatbrennstofföl, das im Bereich von 120 bis 500°C siedet, von 0,0001 bis 0,05 Gew.-%, bezogen auf das Gewicht des Brennstoffs, Polyoxyalkylenestern, -ethern, -ester/ethern oder Mischungen derselben, die mindestens zwei lineare gesättigte C₁₀-C₃₀-Alkylgruppen und ein Polyoxyalkylenglykol mit einem Molekulargewicht von 200 bis 2000 enthalten, wobei die Alkylengruppe des Polyalkylenglykols 1 bis 4 Kohlenstoffatome enthält.

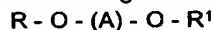
2. Verwendung nach Anspruch 1 für Destillatbrennstofföle, die im Bereich von 200°C ± 50°C bis 340°C ± 20°C siedeten.

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3. Verwendung nach Anspruch 1 oder 2, bei der die lineare gesättigte C₁₀-C₃₀-Alkylgruppe eine C₁₈-C₂₄-Alkylgruppe ist.

4. Mitteldestillatbrennstofföl mit einem Siedebereich von 120 bis 500°C, das 0,0001 bis 0,05 Gew.-% eines Esters, Ethers oder Ester/Ethers oder einer Mischung derselben mit der allgemeinen Formel

50



enthält, in der R und R¹ gleich oder verschieden sind und

(i) n-Alkyl

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sein können, wobei die Alkylgruppe linear und gesättigt ist und 10 bis 30 Kohlenstoffatome enthält und A ein Polyoxyalkylenglykol mit einem Molekulargewicht von 200 bis 2000 ist, wobei die Alkylengruppe 1 bis 4 Kohlenstoffatome enthält.

5. Zusammensetzung nach Anspruch 4, bei der das Brennstofföl ein engsiedender Destillatbrennstoff mit einem Siedebereich von $200^{\circ}\text{C} \pm 50^{\circ}\text{C}$ bis $340^{\circ}\text{C} \pm 20^{\circ}\text{C}$ ist.
6. Zusammensetzung nach Anspruch 4 oder 5, bei der R und R¹ 18 bis 22 Kohlenstoffatome enthalten.
7. Zusammensetzung nach den Ansprüchen 4 bis 6, bei denen das Polyoxyalkylenglykol ein Polyethylenglykol ist.
8. Zusammensetzung nach einem der Ansprüche 4 bis 6, bei der das Glykol eine Mischung von Polyethylen- und Polypropylenglykolen ist.
9. Zusammensetzung nach einem der Ansprüche 4 bis 8, bei der die Säure Behensäure ist und das Glykol ein Molekulargewicht von 200 bis 800 besitzt.
10. Zusammensetzung nach einem der Ansprüche 4 bis 9, die außerdem einen Schmieröfließpunktserniedriger enthält.
11. Zusammensetzung nach Anspruch 10, bei der der Schmieröfließpunktserniedriger ein alkylierter Aromat ist.
12. Destillatbrennstoff, der im Bereich von 120 bis 500°C siedet und 0,0001 bis 0,5 Gew.-% eines Kombinationskaltfließverbesserungsadditivs enthält, das umfaßt
 - (i) einen Ester, Ether, Ester/Ether oder Mischungen derselben mit der allgemeinen Formel

$$\text{R} - \text{O} - (\text{A}) - \text{O} - \text{R}^1,$$
 in der R und R¹ gleich oder verschieden sind und
 - (i) n-Alkyl
 - (ii)
$$\text{n-Alkyl} - \text{C} \begin{array}{c} \text{O} \\ || \end{array}$$
- sein können, wobei die Alkylgruppe linear und gesättigt ist und 10 bis 30 Kohlenstoffatome enthält und A ein Polyalkylenglykol mit einem Molekulargewicht von 200 bis 2000 ist, wobei die Alkylengruppe 1 bis 4 Kohlenstoffatome enthält, und
 - (ii) einen Ethylencopolymer-Paraffinkristallwachstumsinhibitor oder einen öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung-Paraffinkristallwachstumsinhibitor, bei dem es sich um ein Amin- und/oder Amidsalz und/oder Ester/Amid einer Carbonsäure mit 1 bis 4 Carboxylgruppen oder eines Anhydrids davon handelt.
13. Destillatbrennstoff nach Anspruch 12, bei dem das Ethylencopolymer ein Ethylen-Vinylacetat-Copolymer ist.
14. Destillatbrennstoff nach Anspruch 12 und 13, der bezogen auf das Additivgesamtgewicht im Brennstoff 20 bis 40 Gew.-% der Polyoxyalkylenglykolverbindung und 80 bis 60 Gew.-% des Ethylencopolymeren enthält.
15. Destillatbrennstoff nach Anspruch 12, bei dem die polare Stickstoffverbindung das Reaktionsprodukt eines sekundären C₁₂-C₄₀-Amins und Phthalsäureanhydrid ist.
16. Destillatbrennstoff nach Anspruch 15 oder 12, der 20 bis 40 Gew.-% des Esters, Ethers oder Ester/Ethers des Polyalkylenglykols und 80 bis 60 Gew.-% der öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung enthält.
17. Additivkonzentrat zur Einbringung in Destillatbrennstoff, das eine Lösung umfaßt, die 3 bis 75 Gew.-% eines Ester, Ethers oder Ester/Ethers oder Mischungen derselben mit der allgemeinen Formel

$R - O - (A) - O - R^1$,
in der R und R¹ gleich oder verschieden sind und
(i) n-Alkyl

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10 sein können, wobei die Alkylgruppe linear und gesättigt ist und 10 bis 30 Kohlenstoffatome enthält und A ein Polyalkylenglykol mit einem Molekulargewicht von 200 bis 2000 ist, wobei die Alkylengruppe 1 bis 4 Kohlenstoffatome enthält, und außerdem einen Ethylencopolymer-Paraffinkristallwachstumsinhibitor oder einen öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung-Paraffinkristallwachstumsinhibitor, bei dem es sich um ein Amin- und/oder Amidsalz und/oder Ester/Amid einer Carbonsäure mit 1 bis 4 Carboxyl-

15 gruppen oder eines Anhydrids davon handelt, enthält.

18. Additivkonzentrat nach Anspruch 17, das 3 bis 60 Gew.-% des Esters, Ethers, Ester/Ethers oder Mischungen derselben enthält.
- 20 19. Additivkonzentrat nach Anspruch 17 oder 18, das, bezogen auf den Gesamtadditivgehalt des Konzentrats, 60 bis 80 Gew.-% des Ethylencopolymeren oder der öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung enthält.

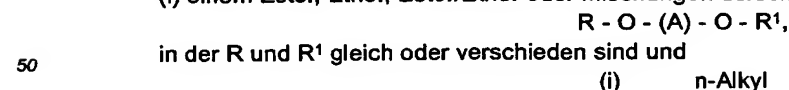
Patentansprüche für folgenden Vertragsstaat : AT

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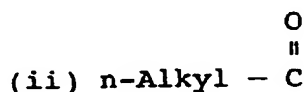
1. Verfahren zur Verbesserung des Kaltfließverhaltens von Destillatbrennstofföl, das im Bereich von 120 bis 500°C siedet, dadurch gekennzeichnet, daß in dieses 0,0001 bis 0,05 Gew.-% eines Polyalkylenesters, -ethers, -ester/ethers oder Mischungen derselben eingebracht werden, die mindestens zwei lineare gesättigte C₁₀-C₃₀-Alkylgruppen und ein Polyoxyalkylenglykol mit einem Molekulargewicht von 200 bis 2000
- 30 enthalten, wobei die Alkylengruppe des Polyoxyalkylenglykols 1 bis 4 Kohlenstoffatome enthält.
2. Verfahren nach Anspruch 1, bei dem das Destillatbrennstofföl im Bereich von 200°C ± 50°C bis 340°C ± 20°C siedet.
3. Verfahren nach Anspruch 1 oder 2, bei dem die C₁₀-C₃₀-Alkylgruppe eine Stearin- und/oder Behengruppe
- 35 ist.
4. Verfahren nach einem der vorangehenden Ansprüche, bei dem das Polyoxyalkylenglykol Polyethylenglykol ist.
5. Verfahren nach einem der vorangehenden Ansprüche, bei dem das Glykol eine Mischung von Polyethylen- und Polypropylenglykolen ist.
- 40 6. Verfahren nach einem der vorangehenden Ansprüche, bei dem außerdem in das Destillatbrennstofföl ein Schmieröfließpunktserniedriger eingebracht wird.
7. Verfahren zur Verbesserung der Kaltfließigenschaften von Destillatbrennstoffen, die im Bereich von 120 bis 500°C siedet, gekennzeichnet durch Einbringung von 0,0001 bis 0,05 Gew.-% einer Kombination von

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- (i) einem Ester, Ether, Ester/Ether oder Mischungen derselben mit der allgemeinen Formel



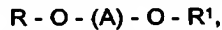
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sein können, wobei die Alkylgruppe linear und gesättigt ist und 10 bis 30 Kohlenstoffatome enthält und

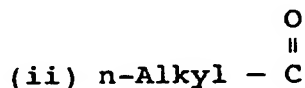
A ein Polyoxyalkylenglykol mit einem Molekulargewicht von 200 bis 2000 ist, wobei die Alkylengruppe 1 bis 4 Kohlenstoffatome enthält, und
 (ii) einem Ethylencopolymer-Paraffinkristallwachstumsinhibitor oder einem öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung-Paraffinkristallwachstumsinhibitor, bei dem es sich um ein Amin- und/oder Amidsalz und/oder Ester/Amid einer Carbonsäure mit 1 bis 4 Carboxylgruppen oder eines Anhydrids davon handelt.

8. Verfahren nach Anspruch 7, bei dem das Ethylencopolymer ein Ethylen-Vinylacetat-Copolymer ist.
9. Verfahren nach Anspruch 7 oder 8, bei dem 20 bis 40 Gew.-% des Polyoxyalkylenglykols und 80 bis 60 Gew.-% des Ethylencopolymeren oder der öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung, bezogen auf das Additivgesamtgewicht in dem Brennstoff, eingebracht werden.
10. Verfahren nach Anspruch 7, bei dem die polare Stickstoffverbindung das Reaktionsprodukt eines sekundären C₁₂-C₄₀-Amins und Phthalsäureanhydrid ist.
11. Verfahren nach einem der vorangehenden Ansprüche, bei dem der Polyoxyalkylenester, -ether oder -ester/ether in den Destillatbrennstoff als eine Öllösung eingebracht wird, die 3 bis 75 Gew.-% eines Esters, Ethers oder Ester/Ethers oder Mischungen derselben mit der allgemeinen Formel



enthält, in der R und R¹ gleich oder verschieden sind und

(i) n-Alkyl



sein können, wobei die Alkylgruppe linear und gesättigt ist und 10 bis 30 Kohlenstoffatome enthält und A ein Polyoxyalkylenglykol mit einem Molekulargewicht von 200 bis 2000 ist, wobei die Alkylengruppe 1 bis 4 Kohlenstoffatome enthält.

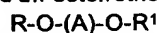
12. Verfahren nach Anspruch 11, bei dem die Öllösung außerdem einen Ethylencopolymer-Paraffinkristallwachstumsinhibitor oder einen öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung-Paraffinkristallwachstumsinhibitor, bei dem es sich um ein Amin- und/oder Amidsalz und/oder Ester/Amid einer Carbonsäure mit 1 bis 4 Carboxylgruppen oder eines Anhydrids davon handelt, enthält.
13. Verfahren nach Anspruch 12, bei dem die Öllösung bezogen auf den Additivgesamtgehalt des Konzentrats 60 bis 80 Gew.-% des Ethylencopolymeren oder der öllöslichen polaren C₃₀-C₃₀₀-Stickstoffverbindung enthält.

Revendications

Revendications pour les Etats contractants suivants : BE, CH, DE, FR, GB, IT, LI, LU, NL, SE

1. Utilisation comme additif améliorant l'écoulement à froid, pour une huile combustible distillée bouillant dans la plage de 120 à 500°C, de 0,0001 à 0,05 % en poids, sur la base du poids du combustible, d'esters, d'éthers, d'esters/éthers polyoxyalkyléniques ou de leurs mélanges contenant au moins deux groupes alkyle saturés linéaires en C₁₀ à C₃₀ et un polyoxyalkylène-glycol ayant un poids moléculaire de 200 à 2000, le groupe alkylène dudit polyoxyalkylène-glycol contenant 1 à 4 atomes de carbone.
2. Utilisation suivant la revendication 1, pour des huiles combustibles distillées bouillant dans l'intervalle de 200 ± 50°C à 340 ± 20°C.
3. Utilisation suivant la revendication 1 ou la revendication 2, dans laquelle le groupe alkyle saturé linéaire en C₁₀ à C₃₀ est en C₁₈ à C₂₄.
4. Huile combustible du type distillat moyen ayant une plage d'ébullition de 120 à 500°C, contenant 0,0001

à 0,05 % en poids d'un ester, d'un éther ou d'un ester/éther ou leur mélange, de formule générale



dans laquelle R et R¹ sont identiques ou différents et peuvent représenter

(i) n-Alkyle

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le groupe alkyle étant linéaire et saturé et contenant 10 à 30 atomes de carbone et A représentant un polyoxyalkylène-glycol de poids moléculaire allant de 200 à 2000, le groupe alkylène contenant 1 à 4 atomes de carbone.

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5. Composition suivant la revendication 4, dans laquelle l'huile combustible est un combustible distillé à plage d'ébullition étroite, ayant une plage d'ébullition de $200 \pm 50^\circ\text{C}$ à $340 \pm 20^\circ\text{C}$.

6. Composition suivant la revendication 4 ou 5, dans laquelle R et R¹ contiennent 18 à 22 atomes de carbone.

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7. Composition suivant les revendications 4 à 6, dans laquelle le polyoxyalkylène-glycol est un polyéthylène-glycol.

8. Composition suivant l'une quelconque des revendications 4 à 6, dans laquelle le glycol est un mélange de polyéthylène- et polypropylène-glycols.

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9. Composition suivant l'une quelconque des revendications 4 à 8, dans laquelle l'acide est l'acide béhénique et le glycol a un poids moléculaire de 200 à 800.

10. Composition suivant l'une quelconque des revendications 4 à 9, contenant également un additif abaissant le point d'écoulement pour huile lubrifiante.

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11. Composition suivant la revendication 10, dans laquelle l'additif abaissant le point d'écoulement pour huile lubrifiante est un composé aromatique alkylé.

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12. Combustible distillé bouillant dans la plage de 120 à 500°C , contenant 0,0001 à 0,05 % en poids d'un additif améliorant l'écoulement à froid qui comprend en association (i) un ester, éther, ester/éther ou leurs mélanges, de formule générale



dans laquelle R et R¹ sont identiques ou différents et peuvent représenter

(i) n-Alkyle

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le groupe alkyle étant linéaire et saturé et contenant 10 à 30 atomes de carbone et A représentant un polyoxyalkylène-glycol de poids moléculaire allant de 200 à 2000, le groupe alkylène contenant 1 à 4 atomes de carbone et (ii) un copolymère éthylénique inhibiteur de croissance des cristaux de cire ou un composé azoté polaire en C₃₀ à C₃₀₀ soluble dans l'huile, inhibiteur de croissance des cristaux de cire, qui est un sel d'amine et/ou d'amide et/ou un ester/amide d'un acide carboxylique ayant 1 à 4 groupes acide carboxylique ou un anhydride de cet acide.

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13. Combustible distillé suivant la revendication 12, dans lequel le copolymère éthylénique est un copolymère d'éthylène et d'acétate de vinyle.

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14. Combustible distillé suivant les revendications 12 et 13, contenant 20 à 40 % en poids du composé de polyoxyalkylène-glycol et 80 à 60 % en poids du copolymère éthylénique sur la base du poids total de l'additif dans le combustible.

15. Combustible distillé suivant la revendication 12, dans lequel le composé azoté polaire est le produit de réaction d'une amine secondaire en C₁₂ à C₄₀ et de l'anhydride phtalique.

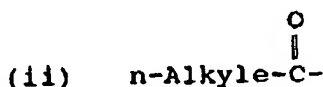
16. Combustible distillé suivant la revendication 15 ou la revendication 12, contenant 20 à 40 % en poids de l'ester, de l'éther ou de l'ester/éther du polyoxyalkylène-glycol et 80 à 60 % en poids du composé azoté polaire soluble dans l'huile en C₃₀ à C₃₀₀.

17. Concentré d'additif destiné à être incorporé dans un combustible distillé comprenant une solution contenant 3 à 75 % en poids d'un ester, éther ou ester/éther ou leurs mélanges de formule générale



dans laquelle R et R¹ sont identiques ou différents et peuvent représenter

(i) n-Alkyle



le groupe alkyle étant linéaire et saturé et contenant 10 à 30 atomes de carbone et A est un polyoxyalkylène-glycol dont le poids moléculaire va de 200 à 2000 et dans lequel le groupe alkylène contient 1 à 4 atomes de carbone, et contenant aussi un copolymère éthylénique inhibiteur de croissance des cristaux de cire ou un composé azoté polaire en C₃₀ à C₃₀₀ soluble dans l'huile, inhibiteur de croissance des cristaux de cire, qui est un sel d'amine et/ou d'amide et/ou un ester/amide d'un acide carboxylique ayant 1 à 4 groupes acide carboxylique ou un anhydride de cet acide.

18. Concentré d'additif suivant la revendication 17, contenant 3 à 60 % en poids de l'ester, éther, ester/éther ou leurs mélanges.

19. Concentré d'additif suivant la revendication 17 ou 18, contenant 60 à 80 % en poids, sur la base de la teneur totale en additif du concentré, du copolymère d'éthylène ou du composé azoté polaire soluble dans l'huile en C₃₀ à C₃₀₀.

Revendications pour l'Etat contractant suivant : AT

1. Procédé pour améliorer l'écoulement à froid d'une huile combustible distillée bouillant dans la plage de 120 à 500°C, qui consiste à incorporer à l'huile 0,0001 à 0,05 % en poids d'un ester, éther, ester/éther polyoxyalkylénique ou leurs mélanges contenant au moins deux groupes alkyle saturés linéaires en C₁₀ à C₃₀ et un polyoxyalkylène-glycol de poids moléculaire compris entre 200 à 2000, le groupe alkylène dudit polyoxyalkylène-glycol contenant 1 à 4 atomes de carbone.

2. Procédé suivant la revendication 1, dans lequel l'huile combustible distillée bout dans l'intervalle de 200 ± 50°C à 340 ± 20°C.

3. Procédé suivant la revendication 1 ou la revendication 2, dans lequel le groupe alkyle saturé linéaire en C₁₀ à C₃₀ est un groupe stéarique et/ou béhérique.

4. Procédé suivant l'une quelconque des revendications précédentes, dans lequel le polyoxyalkylène-glycol est un polyéthylène-glycol.

5. Procédé suivant l'une quelconque des revendications précédentes, dans lequel le glycol est un mélange de polyéthylène- et de polypropylène-glycols.

6. Procédé suivant l'une quelconque des revendications précédentes, qui consiste à incorporer également à l'huile combustible distillée un additif abaissant le point d'écoulement pour huile lubrifiante.

7. Procédé pour améliorer les propriétés d'écoulement à froid de combustibles distillés bouillant dans la plage de 120 à 500°C, qui consiste à incorporer aux combustibles 0,0001 à 0,05 % en poids d'une association (i) d'un ester, éther, ester/éther ou leurs mélanges de formule générale



dans laquelle R et R¹ sont identiques ou différents et peuvent représenter

(i) n-Alkyle



le groupe alkyle étant linéaire et saturé et contenant 10 à 30 atomes de carbone et A représentant un polyoxyalkylène-glycol de poids moléculaire compris entre 200 à 2000, le groupe alkylène contenant 1 à 4 atomes de carbone et (ii) d'un inhibiteur de croissance des cristaux de cire qui est un copolymère d'éthylène ou un composé azoté polaire soluble dans l'huile, en C₃₀ à C₃₀₀, qui est un sel d'amine et/ou d'amide et/ou un ester/amide d'un acide carboxylique ayant 1 à 4 groupes acide carboxylique ou un anhydride de cet acide.

8. Procédé suivant la revendication 7, dans lequel le copolymère d'éthylène est un copolymère d'éthylène et d'acétate de vinyle.

9. Procédé suivant la revendication 7 ou 8, qui consiste à incorporer 20 à 40 % en poids du polyoxyalkylène-glycol et 80 à 60 % en poids du copolymère d'éthylène ou du composé azoté polaire soluble dans l'huile en C₃₀ à C₃₀₀ sur la base du poids total de l'additif dans le combustible.

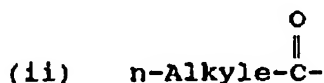
10. Procédé suivant la revendication 7, dans lequel le composé azoté polaire est le produit de réaction d'une amine secondaire en C₁₂ à C₄₀ et de l'anhydride phthalique.

11. Procédé suivant l'une quelconque des revendications précédentes, dans lequel l'ester, l'éther ou l'ester-/éther polyoxyalkylénique est incorporé au combustible distillé sous la forme d'une solution dans une huile contenant 3 à 75 % en poids d'un ester, éther ou ester/éther ou leurs mélanges de formule générale



dans laquelle R et R¹ sont identiques ou différents et peuvent représenter

(i) n-Alkyle



le groupe alkyle étant linéaire et saturé et contenant 10 à 30 atomes de carbone et A étant un polyoxyalkylène-glycol de poids moléculaire compris entre 200 à 2000 dont le groupe alkylène contient 1 à 4 atomes de carbone.

12. Procédé suivant la revendication 11, dans lequel la solution dans l'huile contient également, comme inhibiteur de croissance des cristaux de cire, un copolymère d'éthylène ou un composé azoté polaire soluble dans l'huile en C₃₀ à C₃₀₀ qui est un sel d'amine et/ou d'amide et/ou un ester/amide d'un acide carboxylique ayant 1 à 4 groupes acide carboxylique ou d'un anhydride de cet acide.

13. Procédé suivant la revendication 12, dans lequel la solution dans l'huile contient 60 à 80 % en poids, sur la base de la teneur totale en additif du concentré, du copolymère d'éthylène ou du composé azoté polaire soluble dans l'huile en C₃₀ à C₃₀₀.